

# Mixing and reaction efficiency in closed domains

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# Outline

- 1 Advection - Reaction - Diffusion
- 2 Inert transport
  - Mixing efficiency
  - Flow models
  - Numerical results
- 3 Reactive case
  - Numerical results
- 4 Conclusions

$$\partial_t \theta + \mathbf{u} \cdot \nabla \theta = D \nabla^2 \theta + \frac{1}{\tau_r} f(\theta)$$

2 dim.  $\mathbf{x} = (x, y)$   
 $\theta = \theta(\mathbf{x}, t), \theta \in [0, 1]$

## Assumptions

- **Reaction term:**  $f(\theta) = \theta(1 - \theta)$  (FKPP-like  $\Rightarrow$  pulled fronts);
- **Incompressibility condition:**  
 $\nabla \cdot \mathbf{u} = 0 \Rightarrow \mathbf{u} = (\partial_y \psi, -\partial_x \psi)$ , being  $\psi = \psi(\mathbf{x}, t)$  the stream function;
- **Steep initial condition:**  $\theta(\mathbf{x}, 0) \rightarrow 1$  for  $x \rightarrow -\infty$ ,  
 $\theta(\mathbf{x}, 0) \rightarrow 0$  for  $x \rightarrow +\infty$  (exp. fast);

# Asymptotic situation

(ARD2)

$L$  linear domain size

$$L \gg \ell_0$$

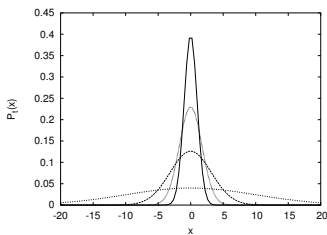
$\ell_0$  typical length of the flow

**front speed:** 
$$V(t) = \frac{1}{L_y \Delta t} \int dx dy [\theta(x, y, t + \Delta t) - \theta(x, y, t)]$$

**effective diffusion coeff.:** 
$$D_{ij}^E = \lim_{t \rightarrow \infty} \frac{1}{2t} \langle (x_i - \langle x_i \rangle)(x_j - \langle x_j \rangle) \rangle$$

$$\begin{aligned} \mathbf{u} = 0 &\Rightarrow V_0 = 2\sqrt{\frac{D}{\tau_r} f'(0)} = 2\sqrt{\frac{D}{\tau_r}} \\ \mathbf{u} \neq 0 &\Rightarrow V_f \leq 2\sqrt{\frac{D^E}{\tau_r}} \quad (D^E \equiv D_{11}^E) \end{aligned}$$

- $D^E$  depends on the velocity field
- Typically:  $D^E \gg D \Rightarrow V_f > V_0$



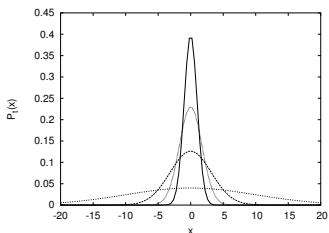
## Inert tracers

$$\mathbf{u} = \mathbf{0}$$

$$\partial_t \theta = D \nabla^2 \theta$$

$$\mathbf{u} \neq \mathbf{0}$$

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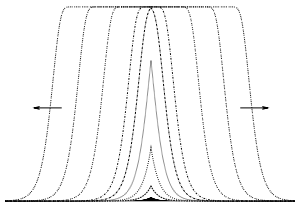
## Reactive particles

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where  $\psi_1$  is time-periodic ( $T$ )  $\implies$  **Lagrangian Chaos**

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$r \ll \ell_0$	$r \gg \ell_0$
$\tau_{m_1} \sim \frac{1}{\lambda} \log \frac{L}{\delta_0} \sim \frac{1}{\lambda}$	$\tau_{m_2} \sim \frac{L^2}{D^E}$
...where...	...where...
$ \delta \mathbf{x}(t)  \simeq  \delta \mathbf{x}(0)  e^{\lambda t}$	$\partial_t \theta = D^E \nabla^2 \theta$

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$ \delta \mathbf{x}(t)  \simeq  \delta \mathbf{x}(0)  e^{\lambda t}$	$\partial_t \theta = D^E \nabla^2 \theta$

let us observe that...

- $\lambda = \lambda(x) \rightarrow$  better to use  $h_{KS} = \int_{\Omega} \lambda(x) d\mu(x)$ ;
- $\tau_{m_1}$  ignores the existence of barriers and the effect of noise ( $D$ );
- $\tau_{m_2}$  is appropriate only if  $L \gg \ell_0$  and ignores transient effects.

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$$A(t) = \frac{1}{N_M} \sum_{i=1}^{N_M} \theta \left( P_i(t) - \frac{c}{N_M} \right); \quad c \sim 0.25$$

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# Meandering-jet

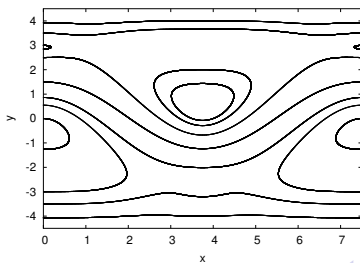
(AD4)

The **stream function** is:

$$\psi(x, y, t) = -\tanh \left[ \frac{y - B(t) \cos kx}{\sqrt{1 + k^2 B(t)^2 \sin^2 kx}} \right] + cy$$

$$B(t) = B_0 + \epsilon \cos(\omega t + \phi)$$

The spatial structure of the stationary flow is:



$$B_0 = 1.2$$

$$k = 4\pi/15$$

$$c = 0.12$$

# Overlap of the resonances

(AD5)

**Cross-stream transport** can be characterized through the **overlap of the resonances criterion**

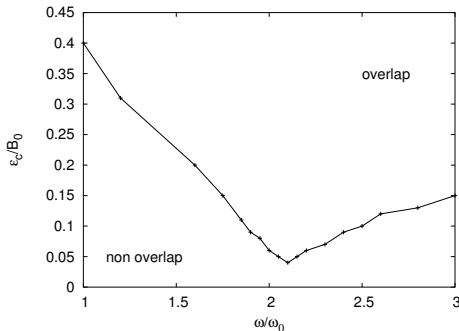
$$\epsilon_c = \epsilon_c(\omega)$$

$\epsilon < \epsilon_c \Rightarrow$  **local chaos**

$\epsilon > \epsilon_c \Rightarrow$  **global chaos**

$$\omega_0 = 0.25$$

$$\phi = \pi/2$$



**Global chaos allows cross-stream transport**

# Stokes flow

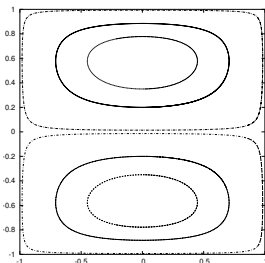
(AD6)

The **stream function** is:

$$\psi(\mathbf{x}, y, t) = \frac{1}{2}[(y + 1) \cos \phi(t) + (y - 1) \sin \phi(t)](1 - x^2)(1 - y^2)$$

$$\phi(t) = 2\pi t/T$$

The spatial structure of the stationary flow is:



$$V_{top} = \cos(\Phi(t))$$

$$V_{bot} = \sin(\Phi(t))$$

$$V_{top}^2 + V_{bot}^2 = 1$$

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# Dispersion of tracers ( $D = 0$ )

(AD7)

**local chaos**

**global chaos**

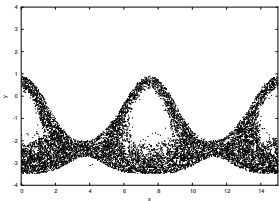
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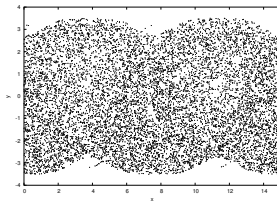
$$\epsilon = 0.03$$



**global chaos**

$$\omega = 0.625$$

$$\epsilon = 0.24$$



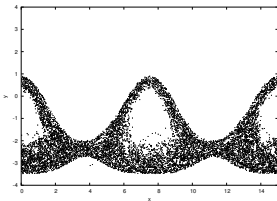
(MJ)

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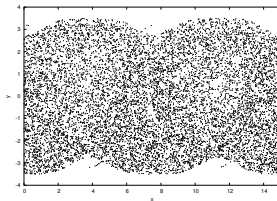
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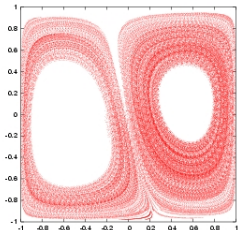
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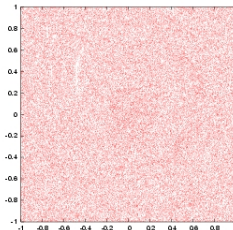


(MJ)

$T = 1$



$T = 16$



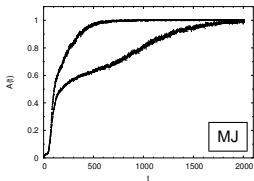
(Stokes)

# Mixing

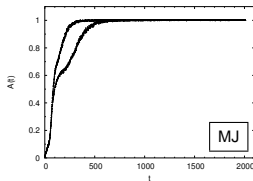
(AD8)

## Occupied area

$D = 0.001$



$D = 0.004$

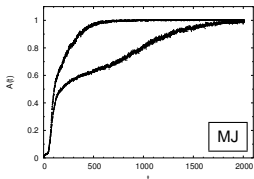


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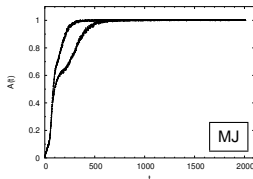
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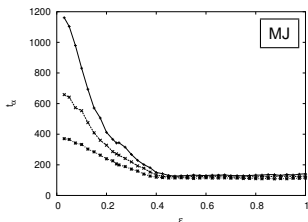


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Mixing times  $t_\alpha$ :  $A(t_\alpha) = \alpha$ ;  $\alpha = 0.9$

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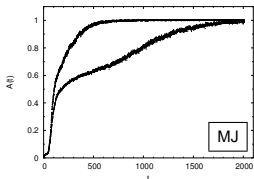
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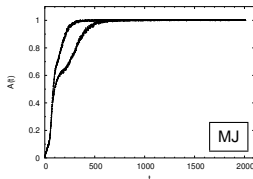
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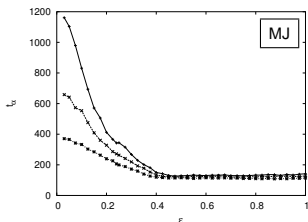


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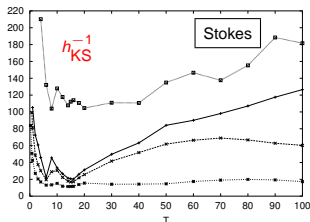
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Discrete-time approach  $\rightarrow$  numerical integration **3-step process:**

- 1 **backward diffusion:**  $\mathbf{x} \rightarrow \mathbf{x} - \sqrt{2D\Delta t} \mathbf{w}$
- 2 **backward advection:**  $\mathbf{x} - \sqrt{2D\Delta t} \mathbf{w} \rightarrow \mathbf{F}_{\Delta t}^{-1}(\mathbf{x} - \sqrt{2D\Delta t} \mathbf{w})$
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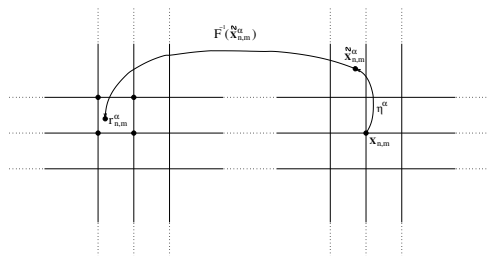
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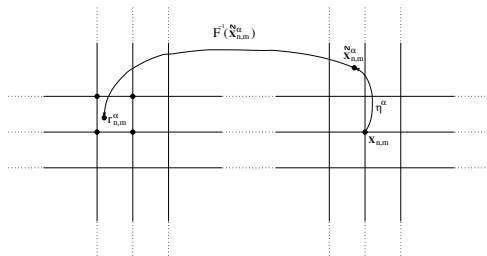
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$$\mathbf{x}(t + \Delta t) = F_{\Delta t}(\mathbf{x}(t)) + \sqrt{2D\Delta t}\mathbf{w}(t) \quad (\text{lagrangian map})$$

$$\theta(t + \Delta t) = G_{\Delta t}(\theta(t)) \quad (\text{reaction map})$$

$$F_{\Delta t}(\mathbf{x}) \simeq \mathbf{x} + \mathbf{u}(\mathbf{x})\Delta t, \quad G_{\Delta t} \simeq \theta + \frac{\Delta t}{\tau_r} f(\theta)$$

$$\theta(\mathbf{x}, t + \Delta t) = \left\langle G_{\Delta t} \left( \theta \left( F_{\Delta t}^{-1}(\mathbf{x} - \sqrt{2D\Delta t}\mathbf{w}(t)), t \right) \right) \right\rangle$$

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- **Asymptotic situation** ( $L_x = 50$   $\omega = 0.4$   $\epsilon = 0.3$   $\tau_r = 2$ )



- In a **non asymptotic situation** the evolution is **not** characterized by **front propagation**



## local chaos

$$L_x = 15$$

$$\omega = 0.625 \quad \epsilon = 0.03$$

$$\tau_r = 2$$

## global chaos

$$L_x = 15$$

$$\omega = 0.625 \quad \epsilon = 0.24$$

$$\tau_r = 2$$

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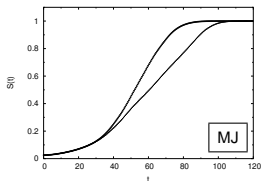
"fresh" material  $\longrightarrow \theta = 0$

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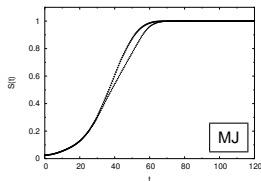
$$\boxed{t_{\alpha} : S(t_{\alpha}) = \alpha} \longleftarrow \text{burning time}$$

## Burnt area

$D = 0.001$

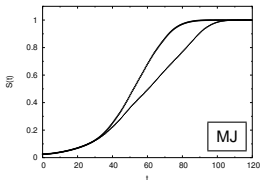


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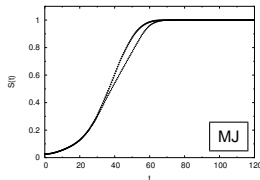


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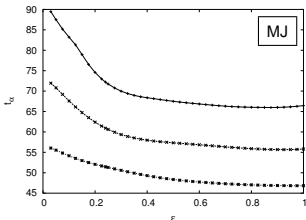


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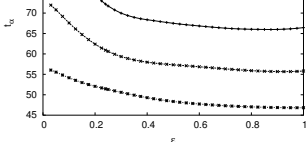


Burning times  $t_\alpha$ :  $S(t_\alpha) = \alpha$ ;  $\alpha = 0.9$

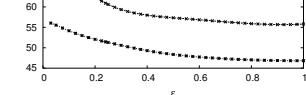
$D = 0.001$



$D = 0.002$

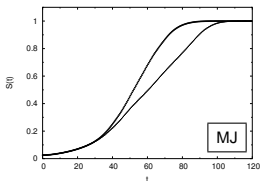


$D = 0.004$

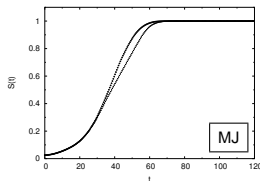


Burnt area

$D = 0.001$

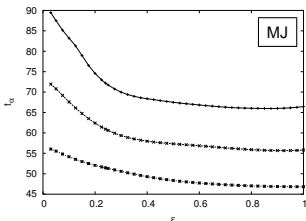


$D = 0.004$



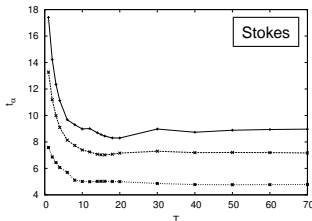
Burning times  $t_\alpha$ :  $S(t_\alpha) = \alpha$ ;  $\alpha = 0.9$

$D = 0.001$



$D = 0.002$

$D = 0.004$



$D = 0.0005$

$D = 0.001$

$D = 0.004$

# Conclusions

## Non asymptotic situation $L \simeq l_0$

- In the **inert case** different dynamical regimes (local or global chaos) imply very different mixing properties.
- **The reactive case** is substantially unaffected by the presence of global chaos. The details of the velocity field have weak influence on the “burning” process, so that a more efficient mixing seems not to imply a better reaction efficiency.

# For Further Reading I

-  M. Cencini, C. López, and D. Vergni  
*Reaction diffusion systems: front propagation and spatial structures in L'heritage de A. N. Kolmogorov en physique*  
published by R. Livi, A. Vulpiani,  
Éditions Belin (2003).
-  M. Abel, A. Celani, D. Vergni and A. Vulpiani  
*Front propagation in laminar flows*  
Phys. Rev. **E 64**, 046307 (2001).
-  G. Boffetta, A. Celani, M. Cencini, G. Lacorata and A. Vulpiani  
*Nonasymptotic properties of transport and mixing*  
Chaos, **10**, 50 (2000).

## For Further Reading II



A. S. Bower

*A simple kinematic mechanism for mixing fluid parcels across a meandering-jet*

J. Phys. Oceanogr. **21**, 173 (1991).



A. Vikhansky

*Control of stretching rate in time periodic flows*

Phys. of fluids **15**, 11, 3342 (2003).



C. López, D. Vergni and A. Vulpiani

*Efficiency of a stirred reaction in a closed vessel*

Eur. Phys. J. **B 29**, 117 (2002).